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# Diffusivity Coefficient of Shogaol Degradation into Paradol in the Reactive Extraction of Ginger Dregs through Subcritical Water

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**Abstract:** The reactive extraction of shogaol and gingerol bioactive compounds using subcritical water is believed to increase diffusivity and selectivity of extraction process. However, a significant problem in extracting shogaol is the thermal degradation of shogaol into paradol under certain process conditions, leading to a reduction in shogaol yield. Therefore, this research aimed to determine diffusivity coefficient of the thermal degradation of shogaol into paradol under certain process. The investigation was conducted in two work stages, namely experimentation and modeling. A mathematical model was developed based on the mass transfer to determine the value of diffusivity (De) in the bulk solution and the micro size of ginger dregs, as well as the reaction speed (k) for the formation of shogaol and paradol. The experiment was conducted at a temperature of  $130^{\circ}$ C and a pressure of 3 bars using subcritical water reactive extractor. Sampling was performed every 10 minutes and the extracts were analyzed using the HPLC. The results showed that diffusivity of gingerol (D<sub>eA</sub>), subcritical water (D<sub>ew</sub>), shogaol (D<sub>eS</sub>), and paradol (D<sub>eP</sub>) was 0.000324 cm<sup>2</sup>/minute, 0.0012 cm<sup>2</sup>/minute, 0.000345 cm<sup>2</sup>/minute, 0.3875 cm<sup>2</sup>/minute, respectively, with a reaction rate constant (k<sup>'''</sup>) of 3.7918 cm<sup>3</sup>/mol/minute.

Keywords: Diffusivity; Extraction; Modeling; Paradol; Subcritical water

## 1. Introduction

Research Article

The use of subcritical water is associated with immense potential during extraction of shogaol reactive and gingerol from ginger dregs (Razak et al., 2023; Yulianto et al., 2022). This subcritical water solvent has polarity equivalent to organic solvents, low viscosity, and surface tension (Cheng et al., 2021). Furthermore, it increases diffusivity by approximately 10 times, reduces hydrogen bonds in water, and improves the rate of mass transfer, particle absorption in the matrix, and the high selectivity of extraction process (Md Sarip et al., 2014; Teo et al. 2010). Despite the numerous advantages, shogaol tends to experience thermal degradation under certain conditions, thereby becoming paradol (Utama-ang et al., 2021; Johnson et al., 2020), with a significant decrease in yield (Handayani et al. 2018; Yulianto et al. 2017).

Paradol, gingerol, and shogaol are compounds that imbue ginger with a spicy and hot taste (Claudya et al., 2023; Ramakrishnan 2013). Similar to shogaol, paradol occurs naturally in ginger but is produced from gingerol transformation due to heating on gingerol (Kamaruddin et al., 2023; Riyadhi et al., 2022; Mao et al., 2019; Rahmani et al., 2014). Bager (2012) stated that under acidic conditions and high temperatures, gingerol changed to shogaol, which was further converted to paradol. In the reaction mechanism at a high temperature and microwave power, 6-gingerol was

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hydrated in structure to 6-shogaol, and reduction occurred  $(CH_2)_2$ , thereby producing paradol (Utama-ang et al., 2021). The attainment of the maximum paradol content had also been observed under the influence of microwave power ranging from 400 to 600 W. Moreover, the optimal conditions for achieving the highest concentrations of 6-gingerol and paradol were determined to be 400 W for 1 minute, producing values of 73.4±1.3 mg/g and 25.5±7.8 mg/g, respectively.

The hydration of shogaol to paradol is a continuation of the reactive extraction process of gingerol from ginger dregs. The mechanism includes the hydration of gingerol to produce shogaol, followed by shogaol to generate paradol at operating temperatures above 130°C (Gonzalez-Gonzalez et al. 2023; Dalsasso et al., 2022; Bhattarai, 2007). Although data regarding the mechanism in the hydration reaction of shogaol to paradol are available, there are still limited reports on diffusivity degradation of the process. Therefore, this modeling research is expected to be carried out using mathematical software without investigating several data because the mathematical parameter values have already been found to minimize paradol formation (Porgo et al., 2019).

Based on the description, this research aimed to determine diffusivity coefficient data of the thermal degradation of shogaol to paradol using subcritical water necessary to direct the reaction that produces shogaol. These data can be used to design process equipment to increase selectivity, improve shogaol yields, and minimize paradol byproducts. Currently, there is no mathematical model regarding the mechanistic reaction of shogaol hydration to paradol. Existing mathematical model is limited to diffusion liquefaction without including simultaneous reaction mechanisms. Therefore, this research discusses the submission of a mechanistic mathematical model from shogaol hydration to mass balance-based paradol.

The novelty of this research is to develop a mathematical model needed to determine the coefficient diffusion during extraction process of paradol, gingerol, and shogaol from ginger. The development is based on mechanistic reaction phenomena which has not been carried out in relation to reactive extraction of ginger dregs. Therefore, the data obtained could be used to confirm relativity with the predicted value.

#### 2. Material and Methods

#### 2.1. Materials

Emprit ginger was purchased from local farmer with a further cleaning process and distilled water was used throughout the entire experiment. Subsequently, formic acid 95% and acetonitrile 99% were purchased from Merck (Bogor, Indonesia). All the chemicals used were of reagent grade unless otherwise showed in this research.

## 2.2. Methods

Subcritical water extraction process in this research with the additional extraction column. Ginger cultivar known as emprit ginger was purified to remove impurities before being subjected to a grated-squeezing machine to obtain a powdered form. Subsequently, ginger powder was dried, ground using a grinder, and filtered through a 50-mesh sieve as raw material. For extraction process, 100 g of ginger dregs powder was combined with 4,000 ml of pure distilled water in a stainless tube equipped with a lid, which served as extraction cell. To ensure the elimination of air and dissolved oxygen, extraction cell was sealed with a stainless lid, and a stream of  $N_2$  gas was introduced for a duration of 2 minutes. Excess pressure was released through a valve and the extractor temperature was gradually increased until it reached 130°C, which was the predetermined condition for extraction process initiation (t = 0). All experiments were conducted under a pressure of 3 bars.

After the completion of extraction process, the resulting extract was quickly transferred to a cooling cell maintained at a temperature of 25°C and a pressure of 1 MPa, facilitating rapid cooling within a duration of 1 minute. Throughout extraction process, multiple samples were collected at regular intervals of 10 minutes. The extracted compounds, specifically shogaol and paradol, present in the continuous phase (water) were subjected to chemical composition analysis using HPLC-MS.

The HPLC-MS system used was a UPLC-QToFMS/MS System manufactured by Water and the LC-MS column used in the analysis was Acquity UPLC BEH C18 1.7um, with dimensions of 2.1x50 mm.

The eluent consisted of two components, namely (A)  $H_2O$  with 0.1% formic acid (Merck) and (B) acetonitrile (Merck) with 0.1% formic acid. The flow rate of the eluent was set at 0.3 mL/min, and the injection was performed at 40 dC with a volume of 5 uL. The MS instrument used was the XEVO-G2QTOF (Water), operating in the resolution mode with electrospray ionization (ESI) in the positive polarity. Subsequently, the data obtained were analyzed using MassLynk software, version 4.1.

## 2.3. Submission of a Mathematical Model

In this research, several assumptions were provided before the submission of a mathematical model. These assumptions include the shape of ginger dregs being a slab, resulting in the distribution of concentration being in the axial position. Furthermore, the state of ginger dregs is unsteady, without influence of temperature and pressure changes (Beverly et al., 2020; Hartati et al., 2020; Porgo et al., 2019; Corrochano et al., 2015), the system is considered fixed, which includes the stationary phase, namely components in ginger dregs and subcritical water as mobile phase. The solvent flow rate, density, and viscosity are assumed to be constant throughout the process, the pressure and temperature gradients are ignored (Ghoreishi and Shahrestani, 2009). Gingerol and shogaol compounds are hydrophobic, thereby the system operates in a heterogeneous phase (Maghraby et al., 2023; Mao et al., 2019).

The reactive extraction mechanism of gingerol with subcritical water in zone one is diffusion. In this zone, subcritical water transport occurs towards the surface of the solid phase (ginger dregs) at a certain speed. In zone two, there is a reaction between subcritical water and gingerol, followed by the reduction of shogaol to paradol reversibly (Ko et al., 2019; Amiri et al., 2018; Jolad et al., 2004). Zone three is the diffusion zone, where gingerol, shogaol, and paradol from the surface of ginger dregs are transported to the liquid phase (Prihutami et al., 2022; Hartati et al., 2020; Yulianto et al., 2020).

The bulk solution model is influenced by several factors, such as the initial concentration of the solute that is uniform throughout ginger dregs (Zhou et al., 2015). Other factors include resistance to mass transfer, the presence of a reaction, the geometry of the solute on the solid surface, the volume of the solution, and the experiment duration (Asl and Khajenoori, 2013). Mathematical models for bulk solutions, such as the diffusion of A from the surface to the core, can be constructed using a mass balance (Lyu et al., 2005).

Input mass rate – Output mass rate + Generational mass rate = Accumulated mass rate (see equation 1)

$$\left(-D_{eW} 2S \operatorname{Nb} \left.\frac{\partial C_W}{\partial x}\right|_{L/2}\right) = V_L \left.\frac{\partial C_{Wf}}{\partial t}\right.$$
(1)

Equation 1 is transformed into equation 2.

$$\frac{\partial C_{Wf}}{\partial t} = -\frac{De_W}{V_L} \cdot 2S. \text{ Nb} \cdot \left(\frac{\partial C_{Wf}}{\partial x}\Big|_{\frac{L}{2}}\right)$$
(2)

With the same method and assumptions, the diffusion of paradol from the core to the surface can be expressed using equation 3

$$\frac{\partial C_{P}}{\partial t} = -\frac{D_{eP}}{V_{L}} \cdot 2S. Nb \cdot \left(\frac{\partial C_{Pf}}{\partial x}\Big|_{\frac{L}{2}}\right)$$
(3)

Initial condition, at  $t = 0 \rightarrow C_W = C_{WO}$ ;  $C_P = 0$ .

In zone two, the reaction occurs between subcritical water and gingerol, while the reduction of shogaol to paradol is reversible, as shown in Figure 1.



**Figure 1** The hydration mechanism of gingerols includes shogaol and paradol which were reported by Utama-ang et al. (2021) and Johnson et al. (2020) with some modification

The proposed mathematical model is based on the phenomenon of the reaction mechanism, as presented with the following denotation: A is gingerol, W is water, E is shogaol, and P is paradol. The reaction can be simplified as follows (equations 4-8):

 $\mathbf{k}_1$ (4) B\* А  $\mathbf{k}_1$  $\mathbf{k}_2$ (5) C\* B\***∢**  $\mathbf{k}_2$  $k_3$ (6)C\* + W ◀ D\*  $k_3$  $\mathbf{k}_4$ (7)D\*◀ Ε  $k_4$ **k**5

$$E \longleftrightarrow P \tag{8}$$

The reaction mechanism in equations 4–8 is arranged to produce the total reaction rate, as presented in equation 9. (9)

$$r_{p} = k_{5} \frac{(k_{4} - k_{-4})}{(k_{5} - k_{-5})} C_{A} - k_{-5} \frac{(k_{4} - k_{-4})}{(k_{5} - k_{-5})} \frac{(k_{1} - k_{-1})}{(k_{4} - k_{-4})} C_{A}$$

Equation (9) is simplified to obtain equation 10.

$$r_{\rm P} = k^{\prime\prime\prime\prime\prime} C_{\rm A} \tag{10}$$

## 2.4. Mass Balance of A in the Volume Element

Input mass rate – Output mass rate + Generation mass rate = Accumulation mass rate. The mass balance of A in the volume element is presented (see equation 11-15).

$$-D_{eA} S \frac{\partial C_A}{\partial x}\Big|_x - \left[-D_{eA} S \frac{\partial C_A}{\partial x}\Big|_{x+\Delta x}\right] - k'''' C_A S \Delta x = S \Delta x \varepsilon \frac{\partial C_A}{\partial t}$$
(11)

the form of equation 11 is solved using limitations to obtain the final result presented in equation 12.

$$\frac{\partial^2 C_A}{\partial x^2} - k^{\prime\prime\prime\prime} C_A = \frac{\varepsilon}{D_{eA}} \frac{\partial C_A}{\partial t}$$
(12)

The values of W, S, and P can be compiled simultaneously through a mass balance. The results of the compilation are presented in Equations 13–15.

$$\frac{\partial^2 C_W}{\partial x^2} - k^{\prime\prime\prime\prime} C_A = \frac{\varepsilon}{D_{eW}} \frac{\partial C_W}{\partial t}$$
(13)

The mathematical model to describe shogaol reactive extraction phenomenon uses Equation 14.

$$\frac{\partial^2 C_S}{\partial x^2} - k^{\prime \prime \prime \prime} C_A = \frac{\varepsilon}{D_{eS}} \frac{\partial C_S}{\partial t}$$
(14)

In this case, paradol acts as the end product of the reactive extraction process. The phenomenon of paradol formation is generally described in a mathematical model, as presented in Equation 15.

$$\frac{\partial^2 C_p}{\partial x^2} + k^{\prime \prime \prime \prime} C_A = \frac{\varepsilon}{D_{eP}} \frac{\partial C_p}{\partial t}$$
(15)

The boundary conditions are  $t = 0 \rightarrow C_A = C_{AO}$ ;  $C_w = C_{wO}$ ;  $C_S = 0$ ;  $C_P = 0$ . Equation 20 shows the initial condition of shogaol. The data used is the fitting result of shogaol extraction with subcritical water at 20 minutes. Boundary conditions are at time  $X=0 \rightarrow \frac{\partial CA}{\partial x} = 0$  and at  $X=X \rightarrow C_A = C_{AO}$ ;  $C_W = C_{WO}$ . To solve the above equation, the calculated parameters used are shown in Table 1

Table 1 Calculated p	parameters
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Parameter	Unit	Value
L	cm	0.4
Nx		20
$V_L$	cm <sup>3</sup>	1000
S	cm <sup>2</sup>	1
Nb		10

#### 3. Results and Discussion

Figure 2 depicts a representative curve showing subcritical water reactive extraction process conducted at a temperature of 130°C and with a pressure of 3 bars. This curve shows the concentrations of gingerol, shogaol, and paradol in the extract as a function of extraction time. Based on the results, it is observed that as extraction time is prolonged, the yield of gingerol, shogaol, and paradol progressively increases. This phenomenon can be attributed to the enhanced contact between the dispersed and the continuous phase (subcritical water), leading to an increased penetration and a greater transfer. However, after the 20-minute mark, the yield of gingerol, shogaol, and paradol shows a reduction due to the degradation of gingerol into shogaol, shogaol into paradol, and paradol into zingerone.



Figure 2 Extraction results compounds of gingerol, shogaol, and paradol

The recovery of gingerol, shogaol, and paradol was observed to increase significantly at a temperature of  $130^{\circ}$ C. Subcritical water acting as a non-polar solvent also served as a catalyst by producing a greater number of ions through the process of water ionization. At  $130^{\circ}$ C, the strength of hydrogen bonds in water significantly reduced, leading to the auto-ionization of water into hydronium ions (H<sub>3</sub>O<sup>+</sup>), which showed acid catalytic properties. Consequently, with a longer extraction time, the dehydration conversion of gingerol to shogaol was enhanced. Ruiz et al. (2013) reported that temperatures above  $150^{\circ}$ C led to weakened hydrogen bonds, causing the auto-ionization of water into hydronium ions (H<sub>3</sub>O<sup>+</sup>) and hydroxide ions (OH<sup>-</sup>), functioning as acid and alkaline catalysts, respectively. Subcritical water also possessed the ability to reduce the activation energy required for extraction process (Peterson et al., 2008).

According to (Mao et al., 2019), shogaol formation occurs under high temperatures for a specific duration. (Wei et al. 2017) proposed that shogaol could potentially revert back to gingerol or experience hydration to form other compounds, such as paradol. This shows the possibility of reducing the concentration of paradol by facilitating the conversion into other derivative compounds, such as zingeron (Sediawan et al., 2023; Mandal et al., 2016; Rahath Kubra et al., 2013; Zhang et al., 2011).

Figures 3 and 4 show the research data and models that refer to equations 3-20 regarding the phenomenon of increasing shogaol and paradol. The results showed that the concentration of shogaol increased as the time was extended. This was because the longer phase contact opportunities and subcritical water conditions led to a reduction in the dielectric constant of water and polarity. Moreover, decreasing the polarity of water can dissolve fewer polar compounds, resulting in a high concentration of solutes (Yulianto et al., 2023).

The results for the proposed model showed that equilibrium occurred at the 20th minute, but there was a decrease in shogaol concentration. This showed that the hydration of shogaol could become paradol compound. According to previous research, significant gingerol dehydration occurred at temperatures above 60°C, with 50% of the degraded sample obtained when the operation period reached 24 hours. Dehydration reactions that run at temperatures above 100°C

will have a faster reaction rate, reaching the equilibrium in a period of 2 hours (Bhattarai et al., 2007).



Figure 3 Comparison of shogaol data and calculations



Figure 4 Comparison of paradol data and calculations

Table 2 shows the values of diffusivity coefficient and the reaction rate constant for the reactive extraction of ginger dregs through subcritical water, validated through a mathematical model. Based on the results, diffusivity of shogaol is higher due to greater molar volume compared to gingerol (Bhattarai et al., 2007). A higher shogaol diffusivity coefficient shows a greater solute transfer rate into the solvent compared to the other components (Teng et al., 2019; Guo et al., 2015; Ghoreishi and Shahrestani, 2009). However, previous research obtained smaller diffusivity values of gingerol and ginger shogaol at extraction temperature of 130°C, which were 8.562 x 10<sup>-11</sup> m<sup>2</sup>/s and 3.886 x 10<sup>-11</sup> m<sup>2</sup>/s, respectively (Anisa et al., 2014).

Table 2 Diffusivity coefficient and reaction rate constant

1	Diffusion in ginger dregs component		
	Diffusivity of gingerol in ginger dregs (D <sub>eA</sub> )	0.0012 cm <sup>2</sup> /minute	
	Diffusivity of subcritical water in ginger dregs (D <sub>eW</sub> )	0.000324 cm <sup>2</sup> /minute	
Diffusivity of shogaol in ginger dregs (DeS)		0.0003435 cm <sup>2</sup> /minute	
	Diffusivity of paradol in ginger dregs (DeP)	0.03875 cm <sup>2</sup> /minute	
2	Reaction Rate		
	Constanta of reaction rate (k''')	0.37918 cm <sup>3</sup> /mol/minute	
3	Dielectric constant (ε)	28.6105	
	SSE	23.06	

Subcritical water diffusivity values in Table 2 show that 0.0012 cm<sup>2</sup>/minute was higher compared to the values obtained by Ghoreishi and Shahrestani (2009). This shows that diffusivity of water in olive leaves is equal to 5.2 x10<sup>-5</sup> m<sup>2</sup>/s. The difference in results is also shown by the dielectric constant ( $\epsilon$ ), which is 49.03, in line with reference value  $\epsilon$  at a temperature of 130°C. Based on the

dielectric constant, the movement of gingerol and shogaol is minimal compared to the reference (Ghoreishi and Shahrestani, 2009).

Notation k	k ''' (cm³/(mol.min))			
ka	0.18959			
kb	0.37918			
kc	0.75836			

**Table 3** Distribution of constant value to measure the limiting step

The limiting step in the reactive extraction mechanism is determined by comparing diffusivity coefficient (D) value with the reaction rate constant (k). The mechanism for constructing the graph includes varying the value of diffusivity coefficient and doubling the reaction rate constant to show the most influential domination. The D and k values for the trial graph are presented in Tables 3 and 4, respectively.



Figure 5 The distribution of the data is dominated by the reaction rate constant (k)

Figure 5 shows the data distribution indicating the dominance of the reaction rate constant (k). Moreover, a decrease in the value of the reaction rate constant influences the resulting calculated data. A smaller value of the reaction rate constant (k) leads to a decrease in the distribution of calculated data and vice versa. When the value of the reaction rate constant is increased, paradol formation value will simultaneously result in a greater concentration.

		2	V		
-	Notation D	$D_{eA}$	$D_{eW}$	$D_{eS}$	$D_{eP}$
_		(cm <sup>2</sup> /min)	(cm <sup>2</sup> /min)	(cm <sup>2</sup> /min)	(cm <sup>2</sup> /min)
	$D_1$	0.00060	0.00016	0.00017	0.01983
	$D_2$	0.0012	0.000324	0.000345	0.3875
	$D_3$	0.00240	0.00065	0.00069	0.07750

Table 4 Distribution of diffusivity value for measuring the limiting step

Table 3 shows the distribution of paradol diffusivity data at a certain scale, as presented in Figure 5. The results show that there is a change in the distribution of concentration data at various diffusivity coefficient values. Specifically, a greater value of diffusivity coefficient affects the increase in the concentration of extraction results. A significant disparity is also observed between Figures 5 and 6, where the effect of diffusivity on extraction process is dominant compared to extraction mechanism.

The calculation of the overall mass transfer coefficient (De) is based on the mass balance equation for subcritical water extraction process. Moreover, it is assumed that the amount transferred is proportional to the concentration difference and the interface area, leading to the proposal of two different model expressions. The first model expression accounts for the particle size of ginger dregs, the total surface area, and the overall absolute mass transfer coefficient (Mandal et al., 2016).



Figure 6 Distribution of diffusivity coefficient (D)

The model's accuracy was evaluated through mean deviation (SSE) by comparing the model data with the experimental data obtained from five independent measurements using ginger dregs model, including  $D_{eA}$ ,  $D_{ew}$ ,  $D_{eS}$ ,  $D_{eP}$ , k, and  $\varepsilon$ . The SSE value for the model describing the reaction mechanism of shogaol to paradol was found to be 23.06.

## 4. Conclusions

In conclusion, this research showed that critical water-assisted extraction carried out at a temperature of 130°C, caused the hydration of the active gingerol compound to become shogaol and paradol. This phenomenon was characterized by a decrease in levels at a certain point in time. The results suggested that diffusivity of gingerol (D\_eA), subcritical water (D\_ew), shogaol (D\_eS), and paradol (D\_eP) in ginger dregs were 0.000324 cm2/minute, 0.0012 cm2/minute, 0.0003435 cm2/minute, and 0.03875 cm2/minute, respectively, with reaction rate constant (k''') of 0.37918 cm3/mol.minute. Based on the data distribution test, diffusivity coefficient in the reactive extraction process showed greater dominancy compared to the reaction rate constant. Furthermore, SSE value showed the potential of the proposed mathematical model to describe the phenomena occurring in the reactive extraction process of ginger dregs.

#### Author Contributions

Mohamad Endy Yulianto: Resources, Investigation, Writing – original draft, Methodology, Formal analysis, Conceptualization, and Software. Bakti Jos: Writing – review & editing, Supervision. Budiyono : Writing – review & editing, Supervision.

#### **Conflict of Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper. The purpose of writing this journal is to develop scientific knowledge, without any duplication of data from other parties' research.

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