

## CYCLE TEMPO POWER SIMULATION OF THE VARIATIONS IN HEAT SOURCE TEMPERATURES FOR AN ORGANIC RANKINE CYCLE POWER PLANT USING R-134A WORKING FLUID

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### ABSTRACT

The focus of this study is an experiment and simulation of an Organic Rankine Cycle (ORC) system to produce electricity. The experimental equipment consisted of four main components: fluid pumps (for refrigerant and water); a condenser as a heat exchanger to condense the working fluid; an evaporator (boiler) as a heat exchanger to evaporate the refrigerant; and an expander (turbine) as a driver to produce electricity. The expander was a modification of a scroll air conditioning (AC) compressor, with a capacity of 1–3 kilowatts and connected to the generator to produce electricity in line with the design estimate. Furthermore, based on the application of the ORC experiment in the form of a small-scale power plant, a pre-determined temperature setting was set for the heat source, ranging between 80 and 100°C. The working fluid used in the study was R-134a. Optimum power estimation was obtained by processing the experimental result data using a software cycle tempo simulation that measured several electrical power outputs between 1.76 and 2.74 kilowatts.

**Keywords:** Expander; Evaporator; Condenser; Cycle Tempo; Organic Rankine Cycle

### 1. INTRODUCTION

Development research on small-scale electricity generation using Organic Rankine Cycle (ORC) system technology has become increasingly prevalent, as seen in the rise in scientific articles on ORC research worldwide. For example, researchers from Belgium, Quoilin et al. (2010), examined the power plant of an ORC system with HCFC-123 working fluid by performing calculation analysis using a numerical system. Chinese researchers Shao et al. (2017) investigated an ORC power plant that also used R-123 as the working fluid on the micro radial flow turbine. Other researchers from Thailand, Sonsaree et al. (2018), examined an ORC integrated with a solar collector as a heat source. A further study by Amicabile et al. (2015) used exhaust heat from diesel engines as a heat source. It is apparent that experiments related to developing ORC for small-scale plant applications have attracted the attention of enthusiastic scientists all around the world. An ORC plant review by Muslim et al. (2015) explains the development of test rigs from the ORC system, while further research by Muslim et al. (2017) focused on the design of the dimensions of the reservoir required to produce hot water to

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evaporate the working fluid in the evaporator. Riyanto and Martowibowo (2015) researched the use of electricity generators was based on the organic Rankine cycle (ORC) system. The purpose of this paper is to establish how much electricity an ORC power plant system uses by employing a cycle tempo simulation program. From the design, based on the results of experiments conducted on the focus of measurement of the main components of the ORC system, it is evident that the evaporator is one of the important components of the ORC system for the production of pressurized working vapor. This allows the pressurized steam to rotate the expander, which is a coupling gen-set for producing electricity. In this field of ORC study, several researchers have conducted ORC generation system experiments by using and modifying a scroll compressor of air conditioning (AC) in car as an expander, employing R-245fa working fluid in the case of Gao et al. (2015) and Ziviani et al. (2014), and R-123 in the case of Wu et al. (2015) and Miao et al. (2015). In this research, the expander from the modification of the scroll AC compressor is used for cooling land vehicles. This study aims to determine the level of thermal efficiency achieved in the experiment. Its originality is the selection of an expander using a Sanden TRSE09 with R-134a working fluid, which is more environmentally friendly.

## 2. METHODS

### 2.1. ORC Theory and Equations

The research methodology used defined several equations specifically devoted to estimating the results of the data processing associated with the experiment ORC on small-scale power plants for organic Rankine cycle (ORC) technology. First, an explanation will be given of the theory of the ORC work process using a P-h diagram, with the working fluid employed being R-134a, as shown in Figure 1.

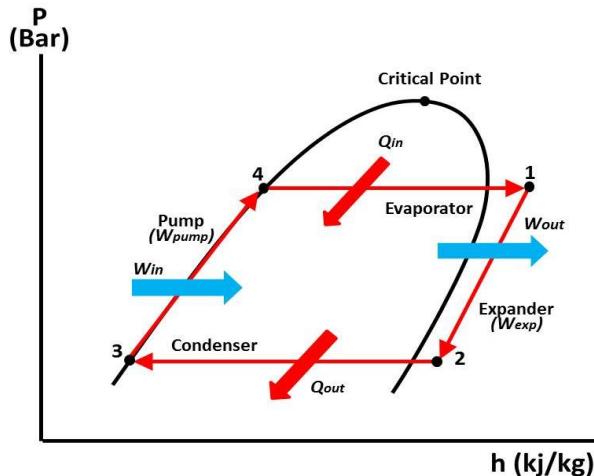


Figure 1 ORC Cycle

Figure 1 explains the process of the ORC system, showing that at point 3 the working fluid pump draws the fluid out of the condenser, which then flows into the evaporator. The pump work rate equation is as follows:

$$W_{Pump} = m_{fluid} \cdot (h_{Pump.out} - h_{Pump.in}) / (\eta_{pump}) \quad (1)$$

or

$$W_p = h_4 - h_3 \quad (2)$$

where  $W_p$  is the power that enters each mass unit by flowing through the pump.

The refrigerant then evaporates in the heat exchanger, which is combined with a heater package to produce hot water. This will release the heat in the flow through refrigerant pipes in the evaporator at positions 1 and 4, enabling the refrigerant to change its phase from liquid to gas. The process of changing the thermal form is the balance of mass and energy given by the following equation:

$$Q_{in} = h_2 - h_3 \quad (3)$$

where  $Q_{in}$  is the rate of heat transfer from the energy source into the working fluid per unit of mass through the evaporator; the refrigerant vapor then flows into the expander.

The refrigerant vapor coming from the evaporator at point 1 is at high temperature and high pressure. It will expand, rotating the expander to produce work, and will then flow to the condenser at point 2 with relatively low vapor pressure.

The heat transfer in on the expander is not taken into account, so the equilibrium rate of mass-energy around the expander is given by the following equation:

$$W_{exp} = h_1 - h_2 \quad (4)$$

where  $W_{exp}$  represents the rate of work produced per unit of steam mass through the expander.

In the condenser, at positions 2 and 3, the heat is ejected through the cooling water pipe at a certain temperature and with a certain amount of heat. The energy equation in the condenser is given as follows:

$$Q_{out} = h_1 - h_4 \quad (5)$$

where  $Q_{out}$  is the rate of energy transfer from the working fluid to the cooling water per unit of fluid mass that works through the condenser. Thermal efficiency is used to measure the amount of energy transferred into the refrigerant by employing the following equation:

$$\eta_{th} = (w_{exp} - w_p)/Q_{in} = ((h_1 - h_2) - (h_4 - h_3)) / (h_1 - h_4) \quad (6)$$

The heat is then released into the environment, so input heat ( $Q_{in}$ ) is essential to the process of increasing heat transfer, while thermal efficiency is reduced. This condition exists due to irreversibility in the pump and expander, meaning the work ( $w_p$ ) needed is greater and the expander work ( $w_{exp}$ ).

## 2.2. Experiment Design

The design of the experimental equipment used in the ORC system is shown in Figure 2, accompanied by a diagram of the ORC apparatus shown in Figure 3. Working fluid enters the evaporator at a given temperature, and is then converted into gas by absorbing the heat from the air in the compartment. The working fluid exits the evaporator as saturated vapor and then enters the compressor. High temperature and high pressure working fluid continues to flow into the condenser and releases heat into the environment. Some of the main ORC equipment, for instance the evaporator, requires a heat source. That used in this study was an electric heater with 1000 kilowatts of power and a maximum temperature of 100°C; it could be set at temperatures of between 80°C and 100°C. Subsequently, to change the working fluid phase in the cooling system and also called a condenser is required.

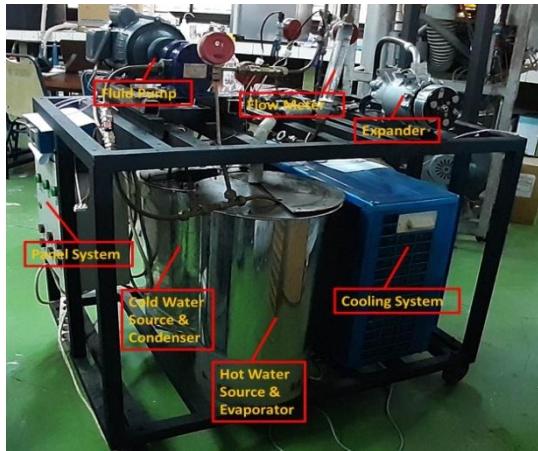


Figure 2 ORC Apparatus

### The Power Generation of Organic Rankine Cycle

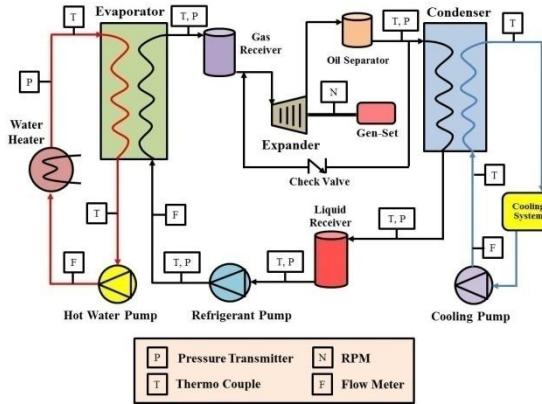


Figure 3 Diagram of ORC

The temperature in this refrigeration system can reach close to 0°C, but for this study it was set at 20°C, to where the goal is to adjust an ambient temperature. The expander is a main component that works as a turbine to drive a generator that will generate electricity. Oralli et al. (2011) conducted an ORC experiment using a scroll compressor type expander from a turbomachine. In this experiment, the expander used was a scroll type Sanden TRSE09. This type of expander is used especially in air conditioning (AC) systems commonly found in cars and can be modified into an expander that drives a generator to produce electricity. The pump used to drain the working fluid in the ORC system is a pump type that is commonly employed for vegetable oil. This working fluid pump is coupled with an electric motor that can adjust to the specifications of other electric motor rotation rates, varying between 500 and 3000 rpm. In this ORC experiment, the working fluid pump was the main component of the ORC system used to drain the working fluid to from all the major components of the ORC system, including the evaporator, expander and condenser. The flow of working fluid allows the main components to work according to their respective functions. The evaporator selected was a type of Plate Heat Exchanger (PHE), which serves to convert the working fluid from liquid to a vapor or gas state. It works by transferring heat energy from the hot water source to the working fluid. The work from a heat source was fresh water which has been heated by a stainless steel heater placed in a water reservoir. The dimensions of the drum including heater with dimension is 60 cm high with a diameter of 50 cm. The water heater could be set up to 100°C. This heating device worked to heat the fresh water, which was used to provide heat to the working fluid to change its liquid state into gas at a certain temperature and display the pressure count on the installed measuring instrument. To enable the fluid to work properly for a refrigeration system was installed in one of component of the ORC experimental equipment. This cooled the fresh water that had been collected in the water reservoir drum. A water pump with an electrical capacity of 370 watts then channelled the flow of cooled water to the condenser. The setting of the cooling water temperature was based on the initial plan, which was 20°C.

### 2.3. Working Fluid Selection

The working fluid used in the experiment was R-134a. This is generally used in a refrigeration system or air conditioning unit to reduce the temperature of the room or to freeze a liquid. In an ORC, the main function of R-134a is as a working fluid that gives momentum to the expander, thereby causing the generator to produce electricity. The specifications of the working fluid used in this experiment are given in Table 1.

Table 1 Properties of R134a

Characteristic	Conditions
Boiling Point	-14.9°F or -26.1°C
Auto-Ignition Temperature	1418°F or 770°C
Ozone Depletion Level	0
Solubility in Water	0.11 % by weight at 77°F or 25°C
Critical Temperature	252°F or 122°C
Cylinder Color Code	Light Blue
Global Warming Potential (GWP)	1200

### 3. RESULTS AND DISCUSSION

From the results of the experiment, it can be seen that the temperature changes of each component of the experimental equipment in the ORC system varied according to the set temperature: 80°C, 85°C, 90°C, 95°C or 100°C.

#### 3.1. Experiment Results

Experiment setting at 80, 85, 90, 95 and 100°C

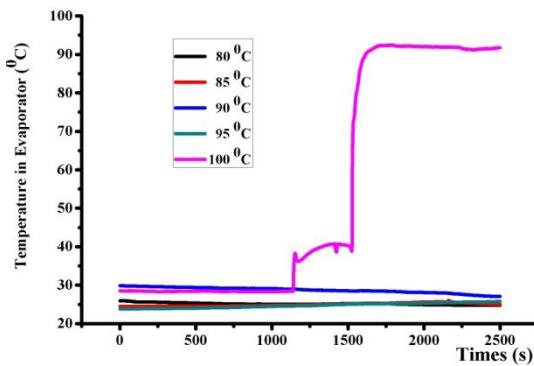


Figure 4 Temperature in Evaporator

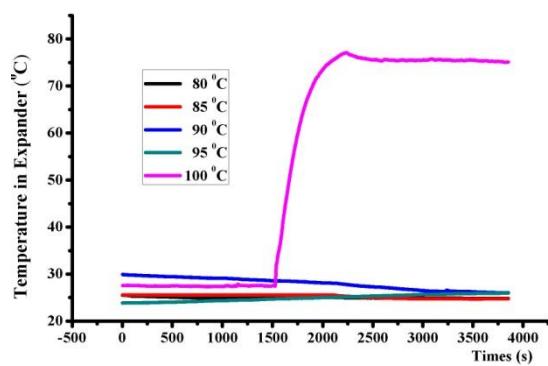


Figure 5 Temperature in Expander

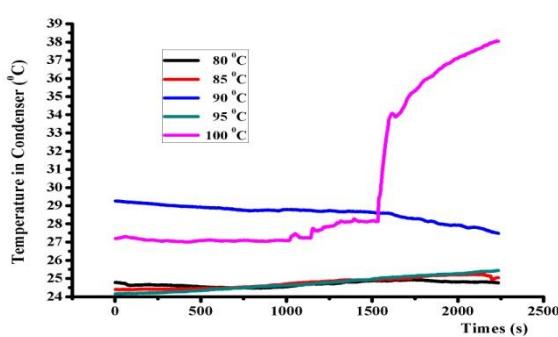


Figure 6 Temperature in Condenser

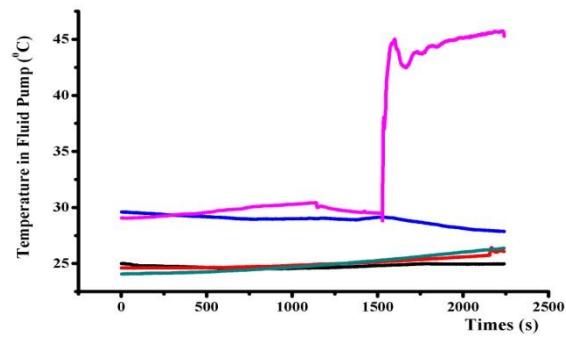


Figure 7 Temperature in Fluid Pump

From each temperature in the evaporator, which has a temperature variation of between 80°C and 100°C, as shown Figure 4, the highest temperature setting chosen was 100°C, because at this level the temperature increases over 1550 to 3500 seconds, based on the results of the measurements from result of the measuring instrument of around 90 to 92°C showed the pressure of the refrigerant can be greatly increased, resulting in the formation of gas in the

working fluid, so there is a strong push into the large expander because there is high enough rotation. The temperature in the expander shown in Figure 5 is the result of data that appeared on the thermocouple display with the highest temperature setting of 100°C and the time position is between 1500 to 2250 seconds with the highest temperature around 75°C. But in this position the temperature becomes somewhat lower due to the release of heat around the expander taken by the ambient temperature. Then in the next process then by setting the temperature variation from 80 to 100°C shown in Figure 6 that can be seen in the highest temperature settings taken is at the setting of 100°C shows that the graph also changes the time process when the seconds to 2250 temperatures at condenser until it can reach 38°C. At this temperature the condition of the working fluid form turns to liquid so that it can be easily flowed by the working fluid pump to the evaporator. The last is in Figure 7 shows that the temperature at the fluid pump based on the highest temperature settings between 80 to 100°C. And also determined that this experiment at a temperature setting of 100°C with temperature output data on a thermocouple display that reads around 45 to 46°C which occurs at 1520 to 2250 seconds. From the explanation of the four main components above which mention the process of increasing and decreasing the temperature of each of the main components, then to make a simulation to estimate the amount of power expander and generator power using software cycle tempo is the setting temperature at 100°C. The choice of setting this temperature of 100°C in order to obtain high power expander and generator power.

### 3.2. Analysis of Actual Experiments

From the five temperature variations of 80°C, 85°C, 90°C, 95°C and 100°C that average temperature obtained from the ORC components includes on temperatures in evaporator, expander and condenser shown at Table 2. Based on the results of the average estimate, the most possible for the best results on the output power obtained is at a setting of 100°C.

Table 2 Average temperature in each component of the ORC system

No.	Temperature (°C) Setting	Average Temperature in Evaporator (°C)	Average Temperature in Expander (°C)	Average Temperature in Condenser (°C)
1.	80	64.36	47.23	26.28
2.	85	70.91	55.60	30.71
3.	90	73.46	55.97	29.99
4.	95	88.44	69.96	28.62
5.	100	91.89	75.51	31.06

### 3.3. Results of Simulation with Cycle Tempo

Based on the data processing variations at five temperature settings, namely from 80°C to 100°C, as shown in Table 2, the data with significant and optimum experimental results are seen in the measurement results. The parameters of the measurement results of the variation of the temperature settings are varied on the heater based on a predetermined temperature that is from 80, 85, 90, 95 and 100°C. Furthermore, the data from the experimental results were entered into program simulation of cycle tempo to as certain how much expander and generator power were simulated. Then based on the simulation results of the cycle tempo with an increase in power of 2.19 kilowatts, 2.33 kilowatts, 2.47 kilowatts, 2.60 kilowatts and 2.74 kilowatts. Then for other parameter measurements is the pressure on some of the main components of the ORC system listed in the cycle tempo simulation that is the pressure on the evaporator at 12 bar and condenser is 6 bar. Both pressures in the evaporator and condenser were set to produce of optimum power in expander and gen-set. The magnitude of the flow rate of working fluid in the ORC system is 0.036 kg/s and the flow of this working fluid greatly affects the amount of energy that occurs in heat transfer in the evaporator and condenser, as well as the magnitude of

the flow affects the power that occurs in the expander and gen-set. The highest temperature dataset will be shown, which affects the size of the components in the ORC system by using a cycle tempo simulation program with the option at of a temperature of 100°C as shown in Figure 8.

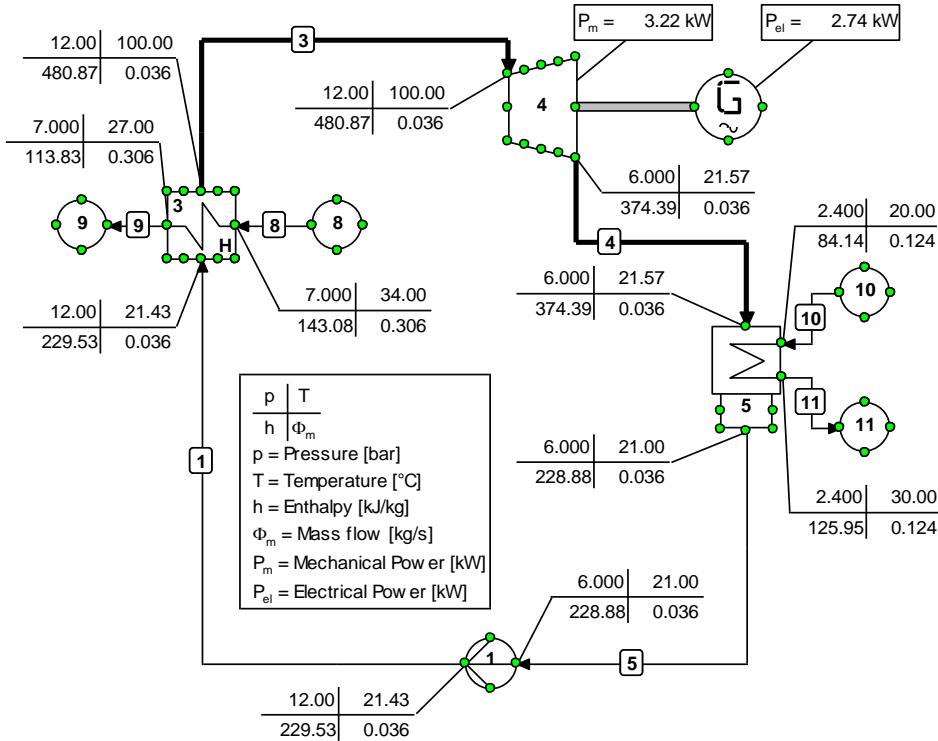


Figure 8 Simulation program of cycle tempo at 100°C

The estimation of the cycle tempo simulation program shows that the temperature setting of 100°C produces estimated electrical power of 2.74 kilowatts.

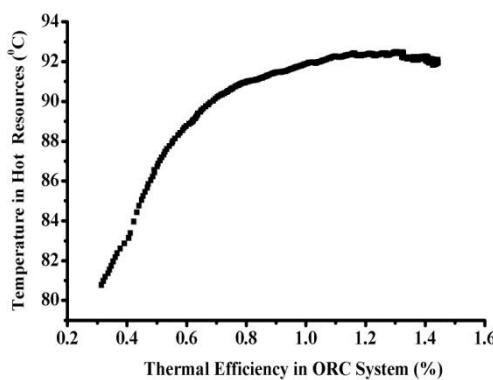


Figure 9 ORC thermal efficiency

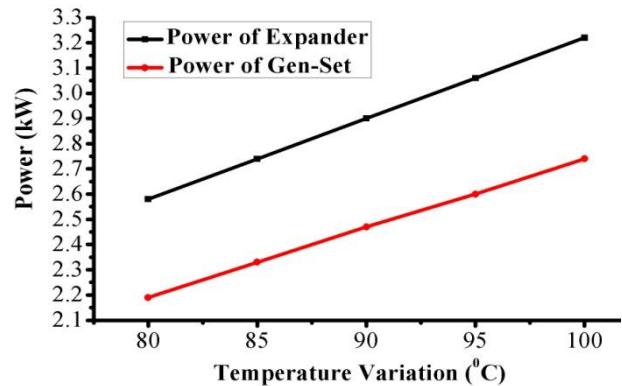


Figure 10 Power ORC with cycle tempo

Figure 9 shows that the increase in the thermal efficiency graph from 0.3% to 1.4% in the ORC system is based on the results of the processed experimental data and is accompanied by an increase in the temperature of the heat source set at 100°C. To predict the magnitude of the expander power and the magnitude of the gen-set power calculated using the cycle tempo simulation program shown in figure 8 selected in setting from 5 temperature variations. Furthermore, the increase in expander and gen-set power based on the cycle simulation of the

sample simulation program results is shown in Figure 10. The results of the cycle tempo simulation show that the greatest increase in expander power was 3.22 kilowatts and in gen-set power 2.74 kilowatts.

#### 4. CONCLUSION

Based on the results of experiments that have been done with processed parameter data such as temperature, pressure and flowrate of working fluid that the refrigerant selected as the working fluid in this ORC system is R-134a. Determination of the variation in temperature set was at 80°C, 85°C, 90°C, 95°C, and 100°C in the installed heat source equipment, and the simulation power estimated by the cycle simulation program was 2.19 kilowatts, 2.33 kilowatts, 2.47 kilowatts, 2.60 kilowatts and 2.74 kilowatts, respectively. Furthermore, the thermal efficiency that occurred during the experimental process was at a temperature setting of 100°C in this ORC system is 0.3–1.4%.

#### 5. ACKNOWLEDGEMENT

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